

Restart of Hot Test for Multi-nuclide Removal Equipment System A

<Reference>

October 28, 2013

Tokyo Electric Power Company

Hot test schedules

- System A: **A hot test restarted on October 28**. Treatment operation will be **stopped temporarily in early November** for modification of the control operation as a measure to prevent “a procedure abnormality and a shutdown of treatment operation”, which occurred on October 4.
- System B: Batch treatment tanks is currently being repaired, and treatment operation is **scheduled to restart in mid-November**
- System C: Currently in operation for **treatment. Treatment operation is (tentatively*) scheduled to be suspended from October 30** for confirmation of corrosion prevention effectiveness, **and to restart in mid-November**. * Subject to change depending on when HIC is replaced.

	October			November			December			Accumulated amount of treated water (as of Oct. 24)
	20	27	3	Mid	Late	Early	Mid	Late		
System A	Installation of sacrificial electrodes			Treatment operation			Corrosion prevention confirmation			10,929m ³
	↓ Filling up with absorbents			↓ Suspension of treatment			Treatment operation			
	↓ Water feeding to the system and check for leakage			↑ Restart of treatment			Treatment operation			
System B	Repair of batch treatment tanks and installation of sacrificial electrodes			Treatment operation			Corrosion prevention confirmation			10,493m ³
				↓ Filling up with absorbents			Treatment operation			
				↓ Water feeding to the system and check for leakage			Treatment operation			
				↑ Restart of treatment			Corrosion prevention confirmation			
System C	Treatment operation			Corrosion prevention confirmation			Treatment operation			4,059m ³
	△ Suspension of treatment (Schedule is subject to change)			Treatment operation			Treatment operation			

■ Outline of the batch treatment tank leakage incident

On June 15, leakage occurred at the batch treatment tank 2A, followed by suspension of treatment operation through the system A on June 16.

- From late June: Cause investigation, and consideration of preventive measures
- From mid-July: Horizontally deployed investigations
- From July: Repair of batch treatment tanks and implementation of corrosion prevention measures to flange parts

On September 25, the cause and preventive actions were announced

On September 27, a hot test for the system C started

- September 28: Shutdown of treatment operation due to clogging of a batch treatment tank of the system C
- October 4: Shutdown of treatment operation after the activation of an alarm indicating a process abnormality at the system C

■ Causes of leakage and corrosion

- Leakage from the lower side of the batch treatment tank 2A was caused by a penetration defect, which resulted from unexpectedly damaging corrosion attributable to **a combination of complex factors: formation of a crevice environment** due to generated iron precipitation; and **development of a corrosive environment** due to injection of chemicals (mainly, hypochlorous acid).
- Further, while **silver impregnated activated carbon** with which the absorption tower 6 is filled is considered to **contribute to occurrence and development of corrosion**, corrosion was found in locations downstream of the absorption tower 6 that are not in the alkaline environment.
- Additionally, around each of the flange parts at inspection openings of the absorption towers, **fluid becomes stagnant, and flows slowly, which is favorable for local corrosion to occur**. This is considered as another factor contributing to development of corrosion.

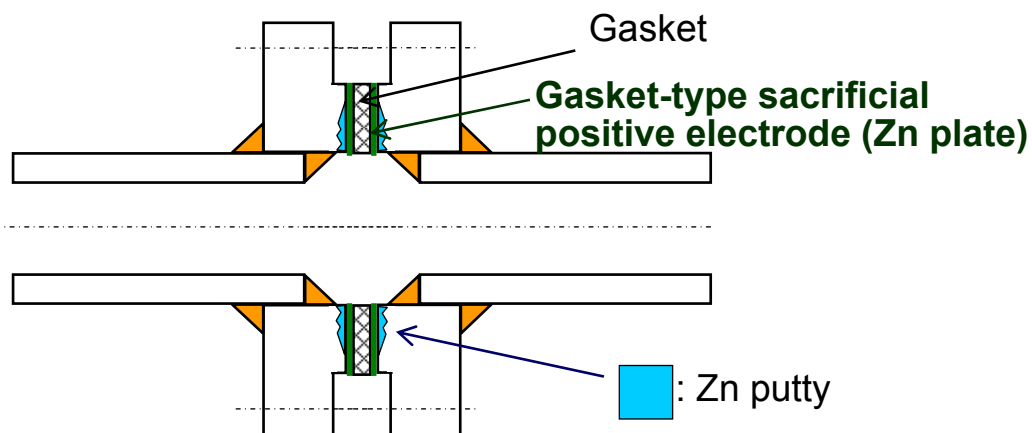
■ Recurrence prevention measures and horizontal deployment

- Recurrence prevention measures on batch treatment tanks

After the damaged parts were repaired, **rubber lining (chloroprene rubber) was provided** on the internal surfaces of the tanks.

- Measures taken within the horizontal deployment range

Gasket-type sacrificial positive electrodes were provided to flanges that have the risk of suffering crevice corrosion (only Zn putty was provided to some of large-diameter flanges). Additionally, for higher reliability, we are considering future **replacement with lining pipes**.



Batch treatment tank 1C
(after rubber lining was provided)



Gasket-type sacrificial positive electrode

■ Preventive actions taken against corrosion in absorption towers

- Bypass the silver impregnated activated carbon tower in a neutral region where a corrosion potential is increased.
- Consider restructuring of absorption towers in order to secure the absorption capability expected from silver impregnated activated carbon, which is to be bypassed.
- Provide sacrificial electrodes to flanges that are likely to suffer crevice corrosion.
- Stop injection of hypochlorous acid
- After the start of a hot test, **regularly inspect** locations corresponding to those in the system A where relatively severe corrosion was found, so that **the effects of the corrosion prevention measures will be checked.** (**Inspections of the system C are scheduled to start on October 30.**)